

(19)



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(11)

EP 0 875 609 A2

(12)

EUROPEAN PATENT APPLICATION

(43) Date of publication:
04.11.1998 Bulletin 1998/45(51) Int. Cl.⁶: D01F 8/06, D04H 1/52,
D04H 1/56

(21) Application number: 98107209.3

(22) Date of filing: 21.04.1998

(84) Designated Contracting States:
AT BE CH CY DE DK ES FI FR GB GR IE IT LI LU
MC NL PT SE
Designated Extension States:
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(30) Priority: 22.04.1997 JP 118895/97

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(54) Fibers and fibrous moldings using the same

(57) The present invention relates to fibers comprising propylene-ethylene copolymer consisting of 0.01 to 15 mol% of ethylene units and 99.99 to 85 mol% of propylene units as at least one component, wherein

a) a chain constitution of the copolymer found by means of nuclear magnetic resonance spectrum has the following relationships:

a-1) in three monomers chain units (triad) in main chains of the copolymer, there is a relationship of formula (I):

$$0.0070 \times C2 - 0.0020 \leq PEP \leq 0.0070 \times C2 + 0.0130 \quad (I)$$

between a fraction of propylene unit - ethylene unit - propylene unit chain (PEP) and a total content of ethylene unit (C2), when PEP being positive, and

a-2) in three monomer chain units (triad) in main chains of the copolymer, there is a relationship of formula (II):

$$0 \leq EEE \leq 0.00033 \times C2 + 0.0010 \quad (II)$$

between a fraction of three continuous ethylene units chain (EEE) and a total content of ethylene unit (C2), as well as

a-3) a ratio of total α,β -methylene carbon atoms (Na β) to total propylene units is within a range of 0 to 1.2 mol%,

b) a weight average molecular weight (Mw) is 50,000 to 1,500,000, as well as

c) a ratio (Mw/Mn) of a weight average molecular weight (Mw) to a number average molecular weight (Mn) is 1.2 to 3.8;

and the use of said fibers in a non-woven fabric, a knitted textile, a filter and an absorbent article.

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Description

Field of the Invention

5 This invention relates to fibers consisting of a specified propylene-ethylene copolymer in which propylene being a major component and fibrous moldings with use of them. In more detail, it relates to fibers and fibrous moldings with use of them which are widely applicable as hygiene materials such as sanitary napkins and throwaway diapers, filtering materials such as air filters and liquid filters, agricultural materials such as insect protecting nets, as well as concrete reinforcing materials.

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Description of the Prior Art

Polyolefin fibers mainly comprising propylene have been hitherto used widely in a hygiene field as surface materials for throwaway paper diapers etc., since they have a light weight, a superior warmth keeping property and a softness, and fibers consisting of propylene-ethylene copolymers which are heat-sealable at a low temperature have been used from the energy saving viewpoint. Recently, non-woven fabrics having more strong and soft physical properties are required as hygiene materials, and fibers consisting of propylene-ethylene copolymers are necessary to be processed under such a temperature condition that fibers being sufficiently softened during adhesive bonding in order to increase a strength. However, if non-woven fabrics being processed at a high temperature, the obtained fabrics are strong but they shrink eminently to form shrimps and also become less soft. Conversely, if non-woven fabrics being processed near the melting points, that is, at the lowest possible temperature region of thermal adhesive processing, the obtained non-woven fabrics become less strong because of insufficient adhesion, so that satisfactory products cannot be obtained. Furthermore, in the cases that non-woven fabrics or cylindrical filters processed from the non-woven fabrics being used under a high temperature circumstance, there are such problems that durability being poor and that a form keeping property and rigidity being lowered.

Thus, since the conventional fibers consisting of propylene-ethylene copolymers have a disadvantage of a low heat resistance, processing and use at a high temperature are limited and so improvement in properties is strongly desired for further enlarging applications.

Furthermore, since the conventional fibers consisting of propylene-ethylene copolymers have a fuming phenomenon owing to low molecular weight oligomers contained in polymers or a breaking phenomenon of threads during spinning, fine fibers is difficultly found and a limitation as to fineness is present.

In Official Gazette of Tokai-Sho 62-156310, fibers consisting of ethylene-propylene random copolymer containing a specified amount of ethylene are disclosed which being superior in a heat roll processability. However, the non-woven fabric with use of them has a disadvantage of poor softness, so that a temperature range for processing into non-woven fabric having sufficient strength and softness for practical uses is very narrow. Thus, there has not been developed any fiber consisting of ethylene-propylene copolymer which satisfies strength and softness.

Problem to be solved by the Invention

40 An object of the invention is to provide fibers consisting of propylene-ethylene copolymer in which propylene being a major component and fibrous moldings with use of them wherein an inherent light weight and softness are kept as well as a thermal resistant characteristic is improved, in view of the above mentioned situation.

Means to solve the Problem

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We inventors have studied eagerly in order to solve the above-mentioned problem and found that fibers having an extremely high heat resistance, a satisfactory strength and softness as well as a good spinning stability can be prepared from propylene-ethylene copolymer having characteristic ethylene chains, an extremely low amount of reverse insertion of propylene monomer units, and a narrow molecular weight distribution, to attain the said object and solve the said problem.

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This invention has the following constitutions.

(1) Fibers comprising propylene-ethylene copolymer consisting of 0.01 to 15 mol% of ethylene units and 99.99 to 85 mol% of propylene units as at least one raw material, wherein

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a) a chain constitution of the copolymer found by means of nuclear magnetic resonance (NMR) spectrum has the following relationships:

a-1) in three monomer chain units (triad) in main chains of the copolymer, there is a relationship of (I):

$$0.0070 \times C2 - 0.0020 \leq PEP \leq 0.0070 \times C2 + 0.0130 \quad (I)$$

between a fraction of three ethylene unit chain (EEE) and a total content of ethylene unit (C2), when PEP being positive, and

a-2) in three monomer chain units (triad) in main chains of the copolymer, there is a relationship of (II):

$$0 \leq EEE \leq 0.00033 \times C2 + 0.0010 \quad (II)$$

between a fraction of three continuous ethylene unit chain (EEE) and a total content of ethylene unit (C2), as well as

a-3) a ratio ($N\alpha\beta$) of total α,β -methylene carbon atoms to total propylene units is within a range of 0 to 1.2 mol%,

b) a weight average molecular weight (Mw) is 50,000 to 1,500,000, as well as

c) a ratio (Mw/Mn) of a weight average molecular weight (Mw) to a number average molecular weight (Mn) is 1.2 to 3.8.

(2) Fibers according to item (1), wherein there is a relationship of formula (III)

$$-8.1 \times C2 + 156.0 \leq Tm \leq -4.4 \times C2 + 165.0 \quad (III)$$

between a melting point of the copolymer (Tm) and a total content of ethylene units (C2).

(3) Fibers according to any of item (1) or (2), wherein fibers are composite fibers in which propylene-ethylene copolymer constitutes at least one component.

(4) A non-woven fabric, wherein fibers according to any of items (1) to (3) being used.

(5) A non-woven fabric according to item (4), wherein the non-woven fabric being a continuous fibrous non-woven fabric obtained by a spun-bonding method.

(6) A non-woven fabric according to item (4), wherein the non-woven fabric being a continuous fibrous non-woven fabric obtained by a melt-blowing method.

(7) A knitted textile, wherein fibers according to any of items (1) to (3) being used.

(8) A filter, wherein fibers according to any of items (1) to (3) being used.

(9) A filter, wherein a non-woven fabric according to any of items (4) to (6) being used.

(10) An absorbent article, wherein a non-woven fabric according to any of items (4) to (8) being used partly.

Mode for Carrying out the Invention

The present invention is illustrated in detail as follows.

As to propylene-ethylene copolymer, a raw material of fibers according to the present invention, the values concerning chain structures of the copolymer, that is a total content of ethylene units (C2), chain unit fractions of monomers (PEP) and (EEE) as well as the number of total α,β -methylene carbon atoms, are calculated from the data measured by ^{13}C -NMR spectra at 67.20MHz and 130°C by using a mixed solution having 8/2 ratio by weight of o-dichlorobenzene/deuterated benzene bromide having a polymer concentration of 20% by weight. As a device for measurement, for example, JOEL-GX270 NMR (made by Nihon Denshi Co. Ltd.) can be used.

Propylene-ethylene copolymers used for fibers according to the invention are copolymers containing 0.01 to 15 mol%, preferably 0.05 to 12 mol%, particularly preferably 0.05 to 10 mol% of ethylene units. If a total content of ethylene units being less than 0.01 mol%, characteristics inherent to the copolymers are lost, and if being above 15 mol%, heat resistance is lowered due to decrease in crystallinity of the copolymer.

Terms "fractional ratio of propylene unit \rightarrow ethylene unit \rightarrow propylene unit (PEP)" and "fractional ratio of three continuous ethylene units (EEE)" as to three-monomers chain units (triad) in main chains of propylene-ethylene copolymer used in the present specification mean that "fractional ratio of propylene unit \rightarrow ethylene unit \rightarrow propylene unit (PEP)" and "fractional ratio of three continuous ethylene units (EEE)" bonded respectively to propylene and ethylene chains as triad units in main chains of propylene-ethylene copolymer determined by a ^{13}C -NMR spectrum method proposed by M. Kakugo et al. (Macromolecules 15, 1150 (1982)). As to fibers according to the invention, peak assignment of ^{13}C -NMR spectra is determined based on the above-mentioned provision by Kakugo et al.

As to propylene-ethylene copolymers used in the present invention, fractional ratio (PEP) of bonded propylene unit \rightarrow ethylene unit \rightarrow propylene unit is a present ratio of chain units of bonded propylene unit \rightarrow ethylene unit \rightarrow propylene unit to all triad chain units in total propylene and ethylene units in main chains of copolymer, in the case of considering three continuous chain units (triad) of monomer. A higher triad fraction (PEP) shows a higher ratio of isolated ethylene units between propylene units, that is, higher randomness.

As to propylene-ethylene copolymers used in the present invention, there is a relationship of formula (I):

$$0.0070 \times C2 - 0.0020 \leq PEP \leq 0.0070 \times C2 + 0.0130 \quad (I)$$

5 between a fractional ratio (PEP) of bonded propylene unit \rightarrow ethylene unit \rightarrow propylene unit and a total content of ethylene units (C2, unit: mol%) if PEP being positive, preferably a relationship of formula (I'):

$$0.0070 \times C2 \leq PEP \leq 0.0070 \times C2 + 0.011 \quad (I').$$

10 and more preferably a relationship of formula (I''):

$$0.0070 \times C2 \leq PEP \leq 0.0070 \times C2 + 0.0090 \quad (I'').$$

15 Propylene-ethylene copolymer having a fraction ratio (PEP) of bonded propylene unit \rightarrow ethylene unit \rightarrow propylene unit excess the above-mentioned formula (I) has not been found within a technical range of the invention. On the other hand, if the (PEP) fractional ratio being below, adhesive property at a low temperature of fibers obtained from the said copolymer becomes poor.

On the other hand, a fractional ratio (EEE) of three continuous ethylene units is a present ratio of chain units of bonded ethylene unit \rightarrow ethylene unit \rightarrow ethylene unit to all triad chain units in total propylene and ethylene units in main chains of copolymer, in the case of considering three continuous chain units (triad) of monomer. The higher the triad fraction (EE) is, the higher the ratio of ethylene units is present as blocks in the copolymer.

As to propylene-ethylene copolymers used in the present invention, there is a relationship of formula (II):

$$0 \leq EEE \leq 0.00033 \times C2 + 0.0010 \quad (II)$$

25 between a fractional ratio (EEE) of bonded ethylene unit \rightarrow ethylene unit \rightarrow ethylene unit and a total content of ethylene units (C2, unit: mol%), preferably a relationship of formula (II'):

$$0.00033 \times C2 - 0.0028 \leq EEE \leq 0.00033 \times C2 + 0.0005, \quad (II')$$

30 and more preferably a relationship of formula (II''):

$$0.00033 \times C2 - 0.0022 \leq EEE \leq 0.00033 \times C2 \quad (II'').$$

35 If the a fractional ratio (EEE) of ethylene unit \rightarrow ethylene unit \rightarrow ethylene unit being excess over the range of the above-mentioned formula (II), a heat seal property at a low temperature of fibers obtained from the copolymer becomes poor. On the other hand, if the (EEE) fractional ratio being below, such copolymer has not been found within a technical range of the invention.

In this specification, a ratio (Na β) of total α,β -methylene carbon atoms to a total content of propylene unit (C3) is a present ratio (Na β , unit: mol%) of total α,β -methylene carbon atoms to a total content of propylene unit (C3) in main chains of propylene-ethylene copolymer determined by ^{13}C -NMR spectra based on a method proposed by T. Tsutsui et al. (POLYMER, 30, 1350 (1989)), and it is 100 times of the numeral value defined as Na β in the said literature. The said value is based on spectra of α,β -methylene carbon atoms owing to an 1,2-insertion reaction of propylene and an insertion reaction of ethylene occurred subsequently after an 2,1-insertion reaction, and reflects a reverse insertion amount of propylene monomer owing to 2,1-insertion reaction of propylene in the copolymer.

In propylene-ethylene copolymers used in the present invention, a ratio (Na β) of total α,β -methylene carbon atoms (unit: mol) to a total content of propylene unit (C3, unit: mol) is within a range of 0 to 1.2 mol%, preferably 0 to 0.5 mol%, and more preferably 0 to 0.2 mol%. If the ratio (Na β) of total α,β -methylene carbon atoms (unit: mol) to total content of propylene unit (C3, unit: mol) being too high, a heat resistance of the copolymer is lowered.

50 Propylene-ethylene copolymers used in the present invention have scarcely reverse insertion of propylene monomer and have a chain structure of copolymer main chains in which ethylene units being bonded more randomly in the copolymer.

A weight average molecular weight (Mw) and a number average molecular weight (Mn) of propylene-ethylene copolymer used in the present invention are based on results determined by using a 0.05% by weight solution of *o*-dichlorobenzene and a mixed polystyrene gel column (for example, PSKgel GMH6-HT made by Toso Co. Ltd.) as a column by gel permeation chromatography (GPC) at 135°C. As a determination device, for example, GPC-150C (made by Water Co. Ltd.) can be used.

Propylene-ethylene copolymer used in the present invention has a weight average molecular weight (Mw) of within

a range of 50,000 to 1,500,000, preferably 100,000 to 1,000,000.

If the weight average molecular weight (Mw) being too high, a melt flow property of the copolymer is decreased to lower a stretching property of thread into fiber, and if being too low, a strength of fiber is lowered.

A ratio (Mw/Mn) of a weight average molecular weight (Mw) to a number average molecular weight (Mn) is 1.2 to 3.8, preferably 1.5 to 3.5.

The said ratio (Mw/Mn) of a weight average molecular weight (Mw) to a number average molecular weight (Mn) is a scale of molecular weight distribution. If the said ratio (Mw/Mn) being too high, a molecular weight distribution becomes too wide and an adhesivity at low temperature of fibers obtained by spinning the said copolymer becomes poor. On the other hand, propylene-ethylene copolymer having a ratio (Mw/Mn) of less than 1.2 has not found within the technology of the present invention.

Propylene-ethylene copolymer used in the present invention has a relationship of formula (III)

$$-8.1 \times C2 + 156.0 \leq Tm \leq -4.4 \times C2 + 165.0 \quad (III)$$

between a melting point of the copolymer (Tm) and a total content of ethylene units (C2, unit: mol%) owing to having these constitutional characteristics, and a relationship of formula (III')

$$-7.2 \times C2 + 156.0 \leq Tm \leq -4.9 \times C2 + 165.0 \quad (III')$$

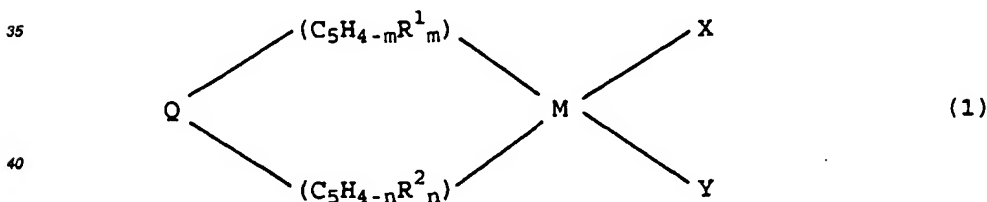
as the case may be according to constitutional conditions, and furthermore a relationship of formula (III'')

$$-6.3 \times C2 + 156.0 \leq Tm \leq -5.4 \times C2 + 165.0 \quad (III'').$$

A melting point is a value of peak temperature showing maximal endothermal amount during melting after increasing a temperature of propylene-ethylene copolymer from the room temperature to 230°C under a temperature increasing condition of 30°C/minute, maintaining the said temperature for 10 minutes, decreasing to -20°C at -20°C/minute, maintaining the said temperature for 10 minutes and melting under a temperature increasing condition of 20°C/minute.

As to preparation method of propylene-ethylene copolymer used in the present invention, there is no particular limitation if the obtained propylene-ethylene copolymer satisfying the above-mentioned conditions, but a preparation method using a specified metallocene catalyst is preferable, wherein a chiral transitional metallic compound as a specific metallocene and aluminoxane are used in combination as a catalyst.

Usable metallocenes are chiral transitional metallic compounds expressed by the general formula (1)



wherein, M is a transitional metallic atom selected from the group consisting of titanium, zirconium and hafnium; X and Y are same or different hydrogen atoms, halogen atoms or hydrocarbon groups; $(C_5H_4-mR^1_m)$ and $(C_5H_4-nR^2_n)$ are substituted cyclopentadienyl groups wherein R^1 and R^2 being same or different hydrocarbon group with 1 to 20 carbon atom(s) optionally bonded with two carbon atoms on cyclopentadienyl ring to form one or more hydrocarbon ring(s) or optionally substituted further with (a) hydrocarbon group(s), or silicon-containing hydrocarbon groups, m and n being an integer of 1 to 3; Q is a two-valent group selected from the group consisting of hydrocarbon group, non-substituted silylene group and hydrocarbon-substituted silylene group which can crosslink $(C_5H_4-mR^1_m)$ and $(C_5H_4-nR^2_n)$.

Chiral transitional metallic compounds of the general formula (1) wherein M is zirconium or hafnium atom, R^1 and R^2 are same or different alkyl groups with 1 to 20 carbon atom(s), X and Y are same or different halogen atoms or hydrocarbon atoms, and Q is dialkyl silylene group are preferable.

As concrete examples of the chiral transitional metallic compounds expressed by the general formula (1), the followings are mentioned: *rac*-dimethyl silylene bis(2-methyl-4,5,6,7-tetrahydroindenyl)zirconium dichloride, *rac*-dimethyl silylene bis(2-methyl-4,5,6,7-tetrahydroindenyl)zirconium dimethyl, *rac*-ethylene bis(2-methyl-4,5,6,7-tetrahydroindenyl)hafnium dichloride, *rac*-dimethyl silylene bis(2-methyl-4-phenylindenyl) zirconium dichloride, *rac*-dimethyl silylene

bis(2-methyl-4-phenylindenyl)zirconium dimethyl, *rac*-dimethyl silylene bis(2-methyl-4-phenylindenyl)hafnium dichloride, *rac*-dimethyl silylene bis(2-methyl-4-naphthylindenyl)zirconium dichloride, *rac*-dimethyl silylene bis(2-methyl-4-naphthylindenyl)zirconium dimethyl, *rac*-dimethyl silylene bis(2-methyl-4-naphthylindenyl) hafnium dichloride, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl)titanium dichloride, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl)zirconium dimethyl, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl)zirconium dimethyl, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl)hafnium dichloride, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl) hafnium dimethyl, dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)titanium dichloride, dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)zirconium dichloride, dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)zirconium dimethyl, dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)hafnium dichloride and dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)hafnium dimethyl.

Amongst of these transitional metallic compounds, the followings are particularly preferable: dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl) zirconium dichloride, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl)zirconium dimethyl, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl)hafnium dichloride, dimethyl silylene(2,4-dimethyl cyclopentadienyl)(3',5'-dimethyl cyclopentadienyl)hafnium dimethyl, dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)zirconium dichloride, dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)zirconium dimethyl, dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)hafnium dichloride and dimethyl silylene(2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl)hafnium dimethyl.

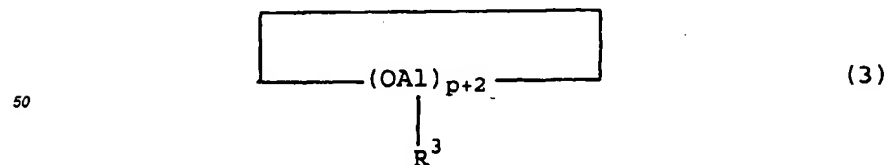
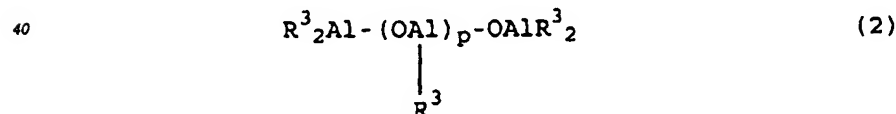
During synthesis of these chiral metallocenes, non-chiral constitutions, i.e. *meso* metallocene compounds, may be produced together, but not all are necessary to be chiral metallocenes in practical use so that *meso* compounds may be mixed in. However, when a mixture with a *meso* compound is used, an atactic polymer from a *meso* compound may be removed by any known method such as a solvent extraction etc. to satisfy the conditions of the invention as to the obtained propylene-ethylene copolymer, according to a mixed amount of the *meso* compound and a copolymerization activity of propylene-ethylene copolymer, as the case may be.

These chiral metallocenes may be used as such to make a catalyst in combination with aluminoxane, or used in supported form on a particulate carrier. As these particulate carriers, granular or spherical particulate solids of inorganic or organic compounds having a particulate diameter of 5 to 300 μ m, preferably 10 to 200 μ m, are used.

As the inorganic compounds used as carriers, there may be mentioned SiO₂, Al₂O₃, MgO, TiO₂ and ZnO etc. as well as these mixtures or composite compounds, for example, SiO₂-Al₂O₃, SiO₂-MgO, SiO₂-TiO₂, SiO₂-Al₂O₃-MgO etc. Amongst of them, those having a main component of SiO₂ or Al₂O₃ are preferable.

Furthermore, as the organic compounds used as carriers, polymers or copolymers of α -olefins such as ethylene, propylene, 1-butene, 4-methyl-1-pentene etc., styrene polymers or copolymers are mentioned.

Aluminoxanes combined as a catalytic component with chiral transitional compounds in a preparation method of propylene-ethylene copolymer used in fibers of the invention are organic aluminium compounds expressed by the general formula (2) or (3).



Wherein, R³ is a hydrocarbon group with 1 to 6, preferably 1 to 4, carbon atoms, for example, an alkyl group such as methyl group, ethyl group, propyl group, butyl group, isobutyl group, pentyl group and hexyl group etc., an alkenyl group such as allyl group, 2-methylallyl group, propenyl group, isopropenyl group, 2-methyl-1-propenyl group and butenyl group etc., a cycloalkyl group such as cyclopropyl group, cyclobutyl group, cyclopentyl group and cyclohexyl group

etc., as well as an aryl group. Amongst of them, an alkyl group is particularly preferable, and each R^3 may be same or different.

p is an integer of 4 to 30, preferably 6 to 30, and particularly preferably 8 to 30.

These aluminosiloxanes may be used alone or in combination with two or more ones. Furthermore, they may be used with alkyl aluminium compounds such as trimethyl aluminium, triethyl aluminium, triisopropyl aluminium, triisobutyl aluminium and dimethyl aluminium chlorides etc.

Aluminosiloxanes can be prepared under various known conditions. Concretely, the following methods may be exemplified.

(1) A method to react trialkyl aluminium directly with water by using an organic solvent such as toluene and ether etc.

(2) A method to react trialkyl aluminium with salts containing water of crystallization such as hydrated copper sulfate hydrate and hydrated aluminium sulfate.

(3) A method to react trialkyl aluminium with water impregnated in silica gel etc.

(4) A method to mix trimethyl aluminium with triisobutyl aluminium and react them directly with water by using an organic solvent such as toluene and ether etc.

(5) A method to mix trimethyl aluminium with triisobutyl aluminium and react them with salts containing water of crystallization such as hydrated copper sulfate hydrate and hydrated aluminium sulfate.

(6) A method to impregnate water in silica gel etc., and react it with triisobutyl aluminium and then trimethyl aluminium.

When the above-mentioned metallocenes and aluminosiloxanes are used in combination as a catalyst in a preparation method of propylene-ethylene copolymer used in fibers according to the invention, respective used amounts of catalyst components are such that aluminium atoms in aluminosiloxanes being within a range of 10 to 100,000 moles per 1 mole of a transitional metallic atom in metallocene, preferably 50 to 50,000 moles, and particularly preferably 100 to 30,000 moles.

Propylene-ethylene copolymer used in the present invention can be prepared by copolymerizing propylene and ethylene in the presence of a catalyst consisting of the above-mentioned combination, and any known (co)polymerization process of propylene may be used as a polymerization method such as a slurry copolymerization method in which propylene and ethylene being polymerized in an inactive solvent, for example, aliphatic hydrocarbons such as butane, pentane, hexane, heptane and isooctane etc., alicyclic hydrocarbons such as cyclopentane, cyclohexane and methylcyclohexane etc., aromatic hydrocarbons such as toluene, xylene and ethyl benzene etc. as well as gasoline fractions and hydrogenated diesel oil fractions; a bulk copolymerization method in which propylene itself being used as a solvent; and a vapor phase copolymerization method in which copolymerization of propylene and ethylene being carried out in vapor phase.

Furthermore, copolymerization can be carried out in any mode of continuous, batchwise or semi-batchwise ones.

For copolymerization of propylene and ethylene, the above-mentioned catalyst may be supplied to a copolymerization reaction system after mixing metallocene and aluminosiloxane previously in an inorganic solvent, or metallocene and aluminosiloxane may be supplied separately to a copolymerization reaction system. Furthermore, before main copolymerization of propylene and ethylene, a minor amount of α -olefin, concretely about 0.001 to 10kg of α -olefin per 1 mole of transition metal in metallocene, may be polymerized in an organic solvent to pre-activate a catalyst consisting of combined metallocene and aluminosiloxane, and then main copolymerization of propylene and ethylene may be carried out, which process is effective for obtaining final propylene-ethylene copolymer in a good particulate form.

As α -olefins useful for pre-activation, α -olefins with 2 to 12 carbon atoms, concretely ethylene, propylene, butene, pentene, hexene, octene and 4-methyl-1-pentene etc. are mentioned, and particularly ethylene, propylene and 4-methyl-1-pentene are used preferably.

When propylene-ethylene copolymers used in fibers according to the invention are obtained by copolymerizing propylene and ethylene in the presence of the above-mentioned catalyst or the pre-activated catalyst by the above-mentioned polymerization processes, copolymerization conditions used are similar to those for propylene polymerization by means of generally known Ziegler-Natta catalysts. That is, propylene and ethylene are supplied in a polymerization vessel at a polymerization temperature of -50 to 150°C, preferably -10 to 100°C, and a polymerization pressure of an atmospheric pressure to 7MPa, preferably 0.2 to 5MPa, and copolymerized for 1 minute to 20 hours.

During copolymerization, a proper amount of hydrogen can be added for control of molecular weight similarly to the

conventional copolymerization processes.

After copolymerization of propylene and ethylene, propylene-ethylene copolymers to be used in fibers of the invention are obtained, if necessary, by known after-treatment procedures such as a catalyst deactivation procedure, a catalyst residue removing procedure and a drying procedure.

5 In the preparation method of propylene-ethylene copolymers used in fibers of the invention by copolymerizing ethylene and propylene in the presence of the above-mentioned catalyst of combined metallocene and aluminoxane, reverse insertion is scarcely formed owing to controlled 1,2-insertion in an insertion reaction of propylene, and on the other hand, ethylene units bond more randomly in the copolymer owing to controlled continuous insertion reaction in an insertion reaction of ethylene.

10 As the result, in the preparation method of propylene-ethylene copolymers, propylene-ethylene copolymer can be obtained having monomer chains with more randomly bonded ethylene units, an extremely low reverse insertion amount of propylene monomer units and a narrow molecular distribution.

In propylene-ethylene copolymers used as a raw material for fibers of the invention, various additives such as an antioxidant, an ultraviolet absorbing agent, an antistatic agent, a nucleating agent, a lubricant, a flame retardant, an anti-blocking agent, a colorant, an inorganic or organic fillers, as well as various synthetic resins may be blended if necessary, in powdery form or using a melt-blending machine, at 190 to 350°C for 20 seconds to 30 minutes, and then supplied as propylene-ethylene copolymer in a pellet form cut into particles.

Furthermore, the specified propylene-ethylene copolymer according to the invention may be mixed with other propylene-ethylene copolymers having a different molecular weight distribution or other copolymers having a similar molecular weight distribution but a different weight average molecular weight, to carry out processing of fibers. Furthermore, other thermoplastic resins may be mixed into in order to carry out processing of fibers without losing efficiency of the invention.

As processing methods of fibers used in the invention, various known spinning methods such as a melt-spinning method, a spun-bonding method and a melt-blowing method are exemplified. By these processing methods, fibers can be converted into multifilaments, monofilaments, staple fibers, tows, webs, non-woven fabrics and knitted fabrics.

Furthermore, a fineness of fibers is not limited particularly and may be any appropriate fineness according to physical properties of used propylene-ethylene copolymer and applications of fibers. For example, in the case of use as hygiene materials represented by absorbent articles such as surface materials of paper diapers and sanitary napkins, surgical cloths and surgical sheets etc., it is preferably 0.1 to 10D. In the case of use as needle punch carpets and tufted carpets etc., it is preferably 8D to 80D. In the case of use as materials of engineering works such as monofilaments, it is preferably 50D to 7000D. Furthermore, in the case of use as filters for fine filtration, extremely fine fibers of about 0.1 to 15µm are preferable.

Fibers of the invention may be subject to crimping if necessary.

35 Webs can be prepared as fibrous webs such as random webs, parallel webs or cross wrap webs etc. by a card or random webber in the case that fibers of the invention being short fibers of more than 20mm or as fibrous web by an airway method or a paper-making method in the case of short fibers having a length of less than 20mm.

A fibrous length is preferably 30 to 150mm in order to orient fibers in a flow direction of a non-woven fabric in the case that fibers being passed through a card or random webber, more preferably 50 to 130mm, with considering a card passing property.

40 The obtained web can be converted into a non-woven fabric by any known processing method for non-woven fabric such as a needle punch method, a thermal roll processing method, a hot-air dryer method, an ultrasonic adhesive method and a high-pressure water flow (water jet) method, and also multiple these processing methods for non-woven fabrics can be combined.

45 Fibers of the invention can be used as a continuous fibrous web obtained by a spun-bonding method or a melt-blowing method etc. The said continuous fibrous web can be converted into a non-woven fabric by using the above-mentioned processing methods for non-woven fabrics.

A basis weight of the non-woven fabric consisting of fibers according to the invention is selected according to the application objects. In the case of using as surface materials of absorbent articles, it is preferably within a range of 5 to 50g/m². In the case of using as materials of engineering works such as drain materials, it is preferably within a range of 50 to 2000g/m². Synthetic fibers such as polyesters etc., natural fibers such as wool etc., and regenerated fibers such as rayon etc. may be mixed into if necessary within a range not interfering the efficiency of the invention.

Furthermore, fibers of the invention can be converted, as such or with other fibers, into primary fibrous products such as knitted woven products and fibrous moldings, by fiber-mixing, mix-spinning, mix-weaving, cross-knitting and cross-weaving.

55 The invention covers fibers spun as single fibers from component consisting of only propylene-ethylene copolymer specified in the invention, as well as covers fibers spun as mono-component fibers from component consisting of the said propylene-ethylene copolymer and other synthetic resins and additives.

The invention covers not only mono-component fibers but also fibers obtained by spinning as mono-component fib-

ers from a component consisting only of propylene-ethylene copolymer specified in the invention, as well as covers fibers obtained by spinning as mono-component fibers from a component consisting of the said propylene-ethylene copolymer specified in the invention or a composition containing it and an other component consisting of synthetic resins by such a way that having cross-section arrangement of a parallel type, a sheath-core type, a eccentric sheath-core type, and a hollow type (called as "composite fiber" or "bi-component fiber"). In this case, as synthetic resins forming the other component, thermoplastic resins are preferable. As thermoplastic resins used as the other component, polyolefin resins, polyester resins and polyamide resins are mentioned, and concretely polypropylene, high-density polyethylene, linear low-density polyethylene, ethylene/propylene copolymer, ethylene/1-buten/propylene terpolymer, polyethylene terephthalate, polybutylene terephthalate, low-melting polyesters obtained by copolymerization of diol and terephthalic acid/isophthalic acid, nylon 6 and nylon 66 etc. are exemplified. In composite fibers according to the invention, particularly in the case of composite fibers of a sheath-core type or a deviated sheath-core type, it is preferable to spin in such a way that a low-melting component being a sheath component. The reason thereof is owing to the fact that a low-melting component of a sheath side is molten by heat to form an adhesive part, in the case of preparation of non-woven fabric by thermal adhesion with using fibers of the invention. Since propylene-ethylene copolymer specified in the invention has a relatively low melting point, composite fibers of a sheath-core type or a deviated sheath-core type spun which have the components containing the said copolymer as a sheath and a thermoplastic resin having a higher melting point than that of the said component as a core are preferable embodiments of the invention, and they have an efficiency of the invention sufficiently. A composite ratio of composite fibers may be optionally selected.

Fibers of the invention have a particularly large effect, either of mono-component fibers or composite fibers, if the said propylene-ethylene copolymer being contained in propylene-ethylene copolymer specified in the invention in an amount of more than 30% by weight, more preferably more than 50% by weight. In the case of not containing other thermoplastic resin as a component, the effect of the invention using propylene-ethylene copolymer specified in the invention is obtained maximally.

Fibers of the invention can be processed secondarily and used widely in a clothing field such as underwear, shirts, blouses, socks, Japanese socks and pantyhose etc.; a bed clothes field such as inside materials, outside materials, sheets, bedcovers, pillow covers and cushions etc.; a medical field such as surgical masks, surgical gowns, caps, doctor's gowns, gauzes and bandages; hygiene materials such as sanitary products, throwaway diapers and urine pads etc.; an interior field such as wallpapers; a field such as inner materials of shoes, intermediate layer and shoes materials; agricultural and gardening materials such as fruit protecting materials and food protecting materials; living articles such as confection wrapping materials, food wrapping materials, cloth wrapping, towels, wet cloths, brushes, table cloths, aprons, kitchen cloths, kitchen gloves, cosmetic puffs, tea bags and wiping cloths; materials of engineering works such as concrete reinforcing materials and draining materials; as well as a filtration material field such as air filters, tobacco filters and liquid filters etc.

Examples

The invention is now illustrated by Examples, but the invention is not limited to the following Examples. Definitions of words and determination methods used in Examples and Comparative Examples are as follows:

- (1) Total content of ethylene units: (unit, mol%) determined by ^{13}C -NMR spectrum
- (2) Triad proportion (PEP):
a proportion of such chains that three-monomer chain unit (triad) in main chains of copolymer being "propylene unit \rightarrow ethylene unit \rightarrow propylene unit" determined by ^{13}C -NMR spectrum
- (3) Triad proportion (EEP):
a proportion of such chains that three-monomer chain unit (triad) in main chains of copolymer being "ethylene unit \rightarrow ethylene unit \rightarrow ethylene unit" determined by ^{13}C -NMR spectrum
- (4) Ratio ($\text{Na}\beta$) of a total α, β -methylene carbon atom number to a total propylene unit content (C3): (unit, mol%)
determined by ^{13}C -NMR spectrum
- (5) Weight average molecular weight (M_w):
determined by GPC
- (6) Number average molecular weight (M_n):
determined by GPC
- (7) Melting point (T_m): (unit: $^{\circ}\text{C}$)
determined by DSC
- (8) Initial tensile resistance: (unit, gf/D)
Longitudinal (MD direction) tensile strength was determined according to JIS L 1015 (1981). However, a part of fibers was determined also at 80°C . A higher initial tensile resistance shows a higher rigidity.
- (9) Average fibrous diameter: (unit, μ)

Five test samples were taken from a web and/or a non-woven fabric after spinning, and photographed by an electronic microscope. One hundred fibrous diameters were determined from the photography and an average value of them was defined as an average fibrous diameter. (10) Strength of non-woven fabric at 5% stretched: (unit, kgf/5cm width)

A non-woven fabric having a width of 5cm was tested by using a tensile strength tester equipped with a temperature controller under such conditions as a clamping distance of 10cm and a tensile speed of 100mm/minute and then converting into a basis weight of the non-woven fabric at 5% stretched, to obtain a strength. A strength of the non-woven fabric was determined in the longitudinal direction (MD direction). The strength was determined at a determination temperature of 20° C and 80°C.

Calculation of strength K into basis weight 20g/m² was carried out by the following formula:

$$K = (20/M) \times Y,$$

wherein M is a basis weight of a non-woven fabric and Y is a strength at 5% stretched.

(11) Strength of non-woven fabric: (unit, kgf/5cm width)

A non-woven fabric having a width of 5cm was tested by using a tensile strength tester equipped with a temperature controller under such conditions as a clamping distance of 10cm and a tensile speed of 100mm/minute, to obtain a break strength after calculated into a value at a basis weight of the non-woven fabric of 20g/m². A strength of the non-woven fabric was determined in longitudinal direction (MD direction). The determination temperature was the room temperature.

Calculation of a strength K into a value at a basis weight 20g/m² was obtained by the following formula:

$$K = (20/M) \times Y,$$

wherein M is a basis weight of a non-woven fabric and Y is a strength at break.

(12) Filtration accuracy: (unit, μm)

One cylindrical filter (250mm) was mounted on a housing of a circulating type filtration tester, and water was recycled from a water tank of 50dm³ via a pump. After controlling a flow amount to 30dm³ per minute, AC fine test dusts (ACFTD) (mean diameter, 6.6 to 8.6μm) were added as test powders to a water tank at 0.5g/minute. After 5 minutes, the original solution and the solution after filtration were sampled. A particulate size distribution of particles contained in respective solutions was determined by using a light cut-off particulate detector. A collecting efficiency showing a ratio of particles collected by the filter was calculated by using the determined result of the particulate size distribution, and a particulate diameter which collected 99.9% was defined as a filtration accuracy.

(13) Pressure resistant strength: (unit, kgf/cm²)

In the above-mentioned filtration accuracy test, one cylindrical filter (250mm) was mounted on a housing of a circulating type filtration tester, AC fine test dusts (ACFTD) (mean diameter, 6.6 to 8.6μm) were added as test powders to a water tank at 0.5g/minute and pressure difference between an inlet side and an outlet side of housing was determined. Addition of powders was continued until the pressure difference of the filter reached to 10(kgf/cm²) or filter was deformed, and the pressure difference at that time was defined as a pressure resistant strength.

(14) Heat resistance:

A cylindrical filter was immersed in warm water having a temperature of 90°C and treated for two hours. Thereafter, a size of the cylindrical filter was determined. Also, change of appearance etc. was observed. Heat resistance was tested on the following basis:

change of size being within 3mm: ○

change of size being over 3mm or strain being recognized in appearance: X

(15) Softness:

A non-woven fabric having a basis weight of 20g/m² was evaluated as to touch based on the following three ranks:

① soft: ○

② normal: △

③ rigid: X

by touch feelings reported by 10 persons (or "monitors"), and an average value of the evaluated results reported by 10 persons (or "monitors") was used as an index of softness.

Preparation method of propylene-ethylene copolymer used in the present invention is illustrated as follows.

Polymerization 1

After an inside of a polymerization vessel having an inside volume of 100dm³ made of stainless steel equipped with a stirrer was substituted with nitrogen gas, 50dm³ of n-hexane, a solution of 2.0mol (calculated as Al atom) of methyl aluminoxane in toluene (made by Toso-Akzo Co. Ltd., trade name: MMAO, concentration: 2mol/dm³), as well as a mixture of 0.09mmol of dimethyl silylene (2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl) hafnium dichloride which being chiral as metallocene and 0.01mmol of a *meso* compound, dimethyl silylene (2,3,5-trimethyl cyclopentadienyl)(2',3',5'-trimethyl cyclopentadienyl) hafnium dichloride were introduced with 0.5dm³ of toluene at 20°C.

Then, after a temperature within the polymerization vessel was raised to 45°C, a mixed gas of 93.9 mol% of propylene, 6.0 mol% of ethylene and 0.1 mol% of hydrogen was supplied continuously into the polymerization vessel while one part of the mixed gas present in a gaseous phase part of the polymerization vessel was exhausted in order to keep a temperature of 45°C and a pressure of 0.4MPa, to carry out copolymerization of propylene and ethylene for 4 hours.

After polymerization was ended, non-reacted propylene, ethylene and hydrogen were discharged from the inside of the polymerization vessel, thereafter 3dm³ of 2-propanol was introduced in the polymerization vessel and stirred at 30°C for 10 minutes, to deactivate the catalyst. Subsequently, 0.2dm³ of aqueous hydrogen chloride solution (concentration: 12mol/dm³) and 8dm³ of methanol were added and heated at 60°C for 30 minutes. After the treatment, stirring was stopped and an aqueous phase part was removed from a lower part of the polymerization vessel, then similar operations were repeated by using the same amounts of an aqueous hydrogen chloride solution and methanol. Then, 0.02dm³ of an aqueous sodium hydride solution (concentration: 5mol/dm³), 2dm³ of water and 2dm³ of methanol were added, and stirred at 30°C for 10 minutes. After the treatment, stirring was stopped and an aqueous phase part was removed from a lower part of the polymerization vessel, then additional 8dm³ of water was added and stirred at 30°C for 10 minutes. After repeating the operation for removing an aqueous phase part twice, polymer slurry was took from the polymerization vessel, filtered and dried, to obtain 2.4kg of propylene-ethylene copolymer, which was used as a sample for evaluation.

Polymerization 2

Propylene-ethylene copolymer was prepared to obtain a sample for evaluation under the same conditions as in Polymerization 1, except that a composition of a mixed gas supplied in a polymerization vessel was 96.8 mol% of propylene, 3.2 mol% of ethylene and 0 mol% of hydrogen and that a polymerization temperature was 50°C.

Polymerization 3

Propylene-ethylene copolymer was prepared to obtain a sample for evaluation under the same conditions as in Polymerization 1, except that n-hexane used in Polymerization 1 as a polymerization solvent was substituted with 50dm³ of toluene and that a composition of a mixed gas supplied in a polymerization vessel was 84.8 mol% of propylene, 15.1 mol% of ethylene and 0.1 mol% of hydrogen.

Polymerization 4

Copolymerization of propylene-ethylene and purification were carried out under the same conditions as in Polymerization 3, except that a mixture of 0.09mmol of dimethyl silylene (2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl) zirconium dichloride which being chiral as metallocene and 0.01mmol of a *meso* compound, dimethyl silylene (2,3,5-trimethyl cyclopentadienyl)(2',3',5'-trimethyl cyclopentadienyl) zirconium dichloride was used and that a composition of a mixed gas supplied in a polymerization vessel was 91.1 mol% of propylene, 8.8 mol% of ethylene and 0.1 mol% of hydrogen, and thereafter the solvent part containing copolymer was removed from the polymerization vessel.

Since the total amount of copolymer was dissolved in the removed solvent, the solution was introduced in a solvent removing device under a reduced pressure, removed off 95% of toluene at 70°C under a reduced pressure, cooled to 25°C, precipitated by introducing 20dm³ of methanol, filtered and dried, to prepare propylene-ethylene copolymer, from which a sample for evaluation was obtained.

Polymerization 5

Propylene-ethylene copolymer was prepared to obtain a sample for evaluation under the same conditions as in Polymerization 1 except that a combination catalyst comprising 0.28mmol as Ti calculation of a titanium catalyst component supported on magnesium chloride, 80mmol of triethyl aluminium and 8mmol of diisopropyl dimethoxy silane as

the third component was used instead of the catalyst (metallocene and methyl aluminoxane) used in Polymerization 1, that 0.5mol of hydrogen was introduced in the polymerization vessel before a mixed gas of propylene and ethylene was supplied in the polymerization vessel, that a mixed gas having a composition of 93.4 mol% of propylene and 6.6 mol% of ethylene was subsequently supplied in the polymerization for 2 hours at such a supplying speed that a polymerization pressure being kept at 0.69MPa without discharging unreacted mixed gas out of the polymerization vessel, and that a polymerization temperature was 60°C.

Polymerization 6

Copolymerization of propylene-ethylene and purification were carried out under the same conditions as in Polymerization 1 except that a mixture of 0.09mmol of *rac*-ethylene bis(indenyl)hafnium dichloride which being chiral as metallocene and 0.01mmol of a *meso* compound, *meso*-ethylene bis(indenyl)hafnium dichloride. When the solvent part containing copolymer was removed from the polymerization vessel, the total amount of copolymer was dissolved in the removed solvent. Then, distilling off the solvent under a reduced pressure, preparation of copolymer by introducing methanol, filtration and drying were carried out similar to Polymerization 4, to obtain propylene-ethylene copolymer, which was used as sample for evaluation.

Example 1

Preparation of fibers and processing thereof into a non-woven fabric were carried out according to the following methods by using the propylene-ethylene copolymer of Polymerization 1, and then physical properties of the obtained fibers were determined and evaluated.

Fibers were produced by using a spinning device equipped with an extruder, a spinneret having a hole diameter of 0.6mm and a winding unit as well as a stretching device equipped multiple heating rolls and a stuffer box type crimper. A non-woven fabric thermally adhered at a relatively low temperature and a non-woven fabric thermally adhered at a relatively high temperature were produced.

Spinning was carried out at a spinning temperature of 280°C and a spinning speed of 964m/minute of the extruder, to obtain non-stretched threads having a single fiber fineness of 3.2D. These non-stretched threads were stretched under such conditions that a temperature of a stretching roll being 40°C and a stretching ratio being 1.5, crimped at 14 peaks/25mm by a crimper, and cut by means of a cutter, to obtain fibers having a single fiber fineness of 2.2D and a fibrous length of 51mm.

These fibers had a single fiber strength of 2.3gf/D, a stretching rate of 311% and an initial tensile resistance of 20gf/D. These fibers were carded by using a carding machine at a speed of 20m/minute, to obtain a web having a basis weight 20g/m². Subsequently, it was adhered thermally by using an embossing roll thermal adhering device with a projection part area of 24% at a temperature of 126°C, to obtain a non-woven fabric. A longitudinal strength of the non-woven fabric was 5.10kgf/5cm width. Similarly, the said carded web was thermally adhered at a temperature of 134°C, to obtain a non-woven fabric. A longitudinal strength of the non-woven fabric was 6.92kgf/5cm width. Softness of the non-woven fabrics thermally adhered at 126 and 134°C is good in both cases.

Therefrom, it can be seen that fibers in Example 1 have a relatively high initial tensile resistance and that the non-woven fabric with use of them has also a high strength after subjected to the high temperature treatment. Evaluated results are shown in Table 1.

Example 2

Processing into a non-woven fabric was carried out according to the following methods by using the propylene-ethylene copolymer of Polymerization 2, and then physical properties of the obtained spun bonded fibers were determined and evaluated.

A spun bonded continuous fibrous fabric was produced by using a spun-bonding device equipped with an extruder, a spinneret having a hole diameter of 0.4mm, an air sucker type drawer, a net conveyor type web collecting unit, a heating machine and a non-woven fabric winding unit etc. As the heating machine, a device equipped with an embossing roll of a thermal adhering device with a projection part area of 11% was used.

A spinning temperature was 230°C and a drawing speed of the air sucker type drawer was 4091m/minute of the extruder. The obtained continuous fibrous web had a single fiber fineness of 1.1D. And, the thermal adhering temperature of the said continuous fibrous web was 134°C.

The said non-woven fabric had a basis weight of 20g/m² and a longitudinal strength of 6.55kgf/5cm width. Furthermore, the said non-woven fabric had a longitudinal tensile strength at 5% stretching of 2.07kgf/5cm width at 25°C and a longitudinal tensile strength at 5% stretching of 1.86kgf/5cm width at 80°C.

The said non-woven fabric had a good tensile strength at 5% stretching at a high temperature. The fabric was supe-

rior in softness, and also strongly superior, to the fabric in Example 1. Furthermore, there was no fuming which lowers a thread stretching property.

Example 3

5

A fine fibrous non-woven fabric was produced by using a melt-blowing device equipped with an extruder, a melt-blowing spinneret having a hole diameter of 0.3mm, a net conveyor type web collecting unit, a calendering device and a non-woven fabric winding unit etc.

10

Propylene-ethylene copolymer of Polymerization 4 was extruded at a spinning temperature in an extruder of 330°C, and the resin extruded from spinning holes was introduced into with hot air heated at 400°C (pressure: 1.9kgf/cm²) and blown onto a web collecting unit of a net conveyor, to obtain a fine fibrous web having a basis weight of about 20g/m² by a melt-blowing method. Heating air which was blown with the web was removed under suction by means of a high-speed air stream suction removing unit equipped at the lower part of the net conveyor. The said web became a non-woven fabric which was molten and adhered by inherent heat during spinning. Physical properties of the non-woven fabric are shown in Table 2.

15

Example 4

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Spinning of melt-blown fine fibers and molding of a cylindrical filter were carried out in continuous methods by using an extruder, a melt-blowing spinneret having a hole diameter of 0.3mm, a net conveyor type web collecting unit, a through air type heating machine and a cylindrical filter molding machine of metal core winding type.

A filter molding machine equipped with an infrared ray type heating unit was used.

25

In order to carry out preparation, propylene-ethylene copolymer of Polymerization 4 was used. The resin was extruded at a spinning temperature in an extruder of 300°C, and the resin extruded from spinning holes was introduced into with hot air heated at 400°C with varying pressure from 0.3 to 2.7kgf/cm² and blown onto a web collecting unit of a net conveyor, to obtain a fine fibrous web having a basis weight of about 50g/m² by a melt-blowing method. Heating air which was blown with the web was removed under suction by means of a high-speed air stream suction removing unit equipped at the lower part of the net conveyor. In order to carry out the melt-blowing spinning, pressure of heating air was changed subsequently in such a way that an inner layer for one filter part being low, a middle layer being high and an outer layer being low.

30

The said web was a density inclining type web wherein fibrous diameter changes respectively from large in the inner layer, via small in the middle layer and to large in the outer layer. The web was heated at a temperature of 115°C by a through-air type heating machine, wound around a metal core of a cylindrical filter molding machine continuously, cooled after a specified outer diameter being attained, and cut into a specified size, to obtain a cylindrical filter in which cross-points of fibers and non-woven fabric layers being melt adhered. Molding was carried out by heating at a temperature of 115°C by means of an infrared heating device during molding. The cylindrical filter had an inner diameter of 30mm, an outer diameter of 70mm and a length of 250mm.

35

Tested results such as a filtering accuracy of the obtained cylindrical filter are shown in Table 2.

Example 5

40

By the similar preparation method to the above-mentioned Example 3, a melt-blown fine fibrous non-woven fabric thermally adhered by pressure was prepared. However, a calendering thermal treatment was used instead of the through-air thermal treatment.

45

Propylene-ethylene copolymer of Polymerization 4 was extruded at a spinning temperature in an extruder of 305°C, and the resin extruded from spinning holes was converted into a melt-blown fine fibrous web having a basis weight of about 25g/m² by introducing heated air at a temperature of 400°C under a pressure of 1.6kgf/cm², which web was then wound continuously on a winding device. The web became a non-woven fabric matter having weak thermal adhesion by inherent heat during spinning.

50

The said non-woven fabric matter was treated at a temperature of 110°C by using a calendering device, to obtain a thermally adhered non-woven fabric. The non-woven fabric had an average fibrous diameter of 0.4μm as well as strength at 5% stretched of 0.85kgf/5cm width at a temperature of 25°C and that of 0.75kgf/5cm width at a temperature of 80°C.

55

This non-woven fabric had a small fibrous diameter, was porous and also was thermally resistant etc., so that it was judged to be useful as a battery separator. Furthermore, this non-woven fabric was judged to be useful as a filter etc. as such or by any after-treatment such as winding or folding etc.

Example 6

A cylindrical filter was molded by using the non-woven fabric obtained in the above-mentioned Example 5. The above-mentioned non-woven fabric was wound around a hollow support made of porous and heat resistant resin to mold a cylindrical filter having an inner diameter of 30mm, an outer diameter of 70mm and a length of 250mm. The non-woven fabric was fixed to the filter at terminal parts having a heat seal width of 4mm.

The filter had a filtering accuracy of 0.6 μ m, a pressure resistant strength of more than 10 and a good heat resistance.

As described above, the cylindrical filter according to the invention was a filter having a good filtering accuracy and a superior heat resistance. The cylindrical filter according to the invention was judged to be useful of course as a filter used at the normal temperature and a filter for filtering at a high temperature, or a filter for foods and medical products after heating and sterilizing treatments etc.

Example 7

A spun-bonded continuous fibrous non-woven fabric was prepared by using propylene-ethylene copolymer of Polymerization 2 by the similar preparation method to Example 2. The copolymer was melt extruded at a spinning temperature in an extruder of 230°C, and the resin extruded from spinning holes were stretched at a speed of 3214m/minute to obtain fibers, which were blown with air onto a net conveyor. Air which was blown was suction removed by an exhausting device equipped on a lower part of a net conveyor. The obtained continuous fibrous web had a single fiber fineness of 1.4D. The said continuous fibrous web was thermally adhered by means of an emboss roll type thermal adhering device at 134° C, to obtain a continuous fibrous non-woven fabric in which fibers being each other thermally adhered with pressure. The said non-woven fabric had a basis weight of 20g/m² and a longitudinal strength of 6.42kgf/5cm width. Furthermore, the said non-woven fabric had a 5% longitudinal tensile strength of 2.03kgf/5cm width at 25°C and a 5% longitudinal tensile strength of 1.79kgf/5cm width at 80°C.

The said non-woven fabric had a good longitudinal tensile strength at 5% stretching at a high temperature.

Example 8

Thermally molten adhesive composite fibers were prepared by the similar preparation method to Example 1. However, as a composite spinning device, there was used a composite spinning device equipped with two extruders and sheath-core type composite spinnerets having a hole diameter of 0.6mm. Spinning was carried out at a spinning temperature of 305°C by using propylene-ethylene copolymer of Polymerization 1 as a sheath component and polyethylene terephthalate having a melting point of 255°C as a core component. Non-stretched threads having a single fiber fineness of 3.2D were obtained by spinning at a melt extruding speed of 924m/minute and a ratio of a sheath component weight to a core component weight of 4:6 (a composite ratio), which threads were then stretched under such conditions as a stretching roll temperature of 95° C and a stretching ratio of 1.5, crimped at 15 peaks/25mm by a crimper and thereafter cut, to obtain short fibers having a single fiber fineness of 2.2D and a fibrous length of 51mm. The said fibers had a single fiber strength of 3.0gf/D, a stretching degree of 202% and an initial tensile resistance of 28gf/D.

The said short fibers were thermally adhered with pressure by means of a carding and emboss roll type thermal adhering device, to obtain two kinds of non-woven fabrics thermally adhered at different temperatures.

The non-woven fabric obtained at a thermal adhering temperature of 126°C had a basis weight of 20g/m² and a longitudinal strength of 5.55kgf/5cm width. And, the non-woven fabric obtained at a thermal adhering temperature of 134°C had a basis weight of 20g/m² and a longitudinal strength of 6.68kgf/5cm width.

The composite fibers became thermally adhesive by a thermal treatment at a temperature between higher than a softening point of the sheath component and lower than a melting point of the core component, as well as had a high single fiber strength and a high initial tensile resistance. Furthermore, the thermally adhered non-woven fabrics with use of the said composite fabric were the strong fabrics concerning to both of treated at low and high temperatures. Furthermore, softness was also good. However, there was found fuming around spinnerets but slightly.

Example 9

The non-woven fabric obtained at a thermally adhering temperature of 126°C in the above-mentioned Example 8 was used to prepare an absorbent article.

Adult paper diaper was used, and only a surface material of the said paper diaper was substituted with the non-woven fabric from the above-mentioned Example 6. The said paper diaper originally consisted of a surface material of polypropylene spun-bonded non-woven fabric having a basis weight of 21g/m², an absorbing material in which pulp and highly absorbing resin being mixed, as well as a backing material of fine porous polyethylene film, wherein the said

absorbing material was wrapped with pulpy tissue as well as the above-mentioned surface material and backing material were made as heat-sealed constitutions against their surroundings.

The surface material was removed from the paper diaper, to which the non-woven fabric of the above-mentioned Example 8 was laminated. Furthermore, at both side positions near leg parts between the above-mentioned surface material and the backing material, each three polyurethane elastic threads were clamped and thermally adhered near surroundings of the above-mentioned surface material and backing material. The remainder of the surface material was cut by scissors and removed, to make a paper diaper with use of the non-woven fabric consisting of thermally adhering composite fibers. Since the said paper diaper was curved in an approximately bow form due to polyurethane elastic threads arranged near both leg parts and also the surface material had a high strength, there could be made a superior product as an adult paper diaper. Since the surface material of the said paper diaper was very flexible, it had a soft touch.

Example 10

Composite monofilaments were prepared by using a composite monofilament manufacturing device equipped with two extruders, sheath-core type composite spinnerets having a bore diameter of 1.0mm, a warm water bath and a stretching machine.

Propylene-ethylene copolymer of Polymerization 3 used as a sheath component and polyethylene terephthalate having a melting point of 34°C used as a core component were spun into water of 34°C at a spinning temperature of 300°C, to obtain non-stretched composite monofilaments having a single fiber fineness of 1750D. The said non-stretched threads were spun and stretched continuously under such conditions as the first and the second stretching temperatures of 105°C, a warm water bath temperature of 96°C and a stretching ratio of 7.0, to prepare composite monofilaments. The obtained composite monofilaments had a ratio of a sheath component weight to a core component weight of 4:6, a single fiber fineness of 251D, a monofilament strength of 6.9gf/D, a stretching rate of 35% and an initial tensile resistance of 45gf/D. Furthermore, the fibers had an initial tensile resistance of 37gf/D at 80°C.

The said composite monofilaments had a thermal adhesiveness, a high strength and a high initial tensile resistance, particularly a high initial tensile resistance at a high temperature.

Example 11

A net in which cross-points of fibers being thermally adhered was prepared as follows by using a net manufacturing device equipped with a weaving machine and a hot through air type heater.

A net having a weaving density of 9 warps/50mm and 9 wefts/50mm was woven by using composite monofilaments of the above-mentioned Example 10 as warps and wefts and heated at a temperature condition of 155°C, to prepare a net in which cross-points of fibers being thermally adhered. Thermal treatments for weaving and thermal adhesion of the net were carried out continuously.

A strength in a longitudinal direction of the obtained net was 8.57kgf/5cm width.

The said net was judged to be preferably useful as an agricultural housing cover material, a protective nets for engineering work and an intermediate material such as filter when used alone or together with other products such as other non-woven fabrics and moldings of synthetic resins.

Comparative Example 1

Propylene-ethylene copolymer of Polymerization 5 was processed into fibers and physical properties of the obtained fibers were determined and evaluated by a similar method to Example 1. As the result, fibers having a single fiber fineness of 2.2D were obtained. The fibers had a single fiber strength of 1.2gf/D, a stretching rate of 314% and an initial tensile resistance of 9gf/D. The fibers were subject to carding and thermal adhesive treatments, to obtain a non-woven fabric having a basis weight of 20g/m². The non-woven fabric obtained at a thermal adhesion temperature of 126°C had a longitudinal strength of 4.00kgf/5cm width and one obtained at a thermal adhesion temperature of 134 °C had a longitudinal strength of 3.91kgf/5cm width. Softness of the non-woven fabric was normal at a thermal adhesion temperature of 126°C, but became hard at 134°C. Furthermore, fuming could be confirmed near spinnerets.

Therefore, it was seen that the fibers of Comparative Example 1 had a relatively low initial tensile resistance and that the non-woven fabric with use of the fibers had a decreased strength in the case of a high temperature treatment being carried out. Evaluated results are shown in Table 1.

Comparative Example 2

Propylene-ethylene copolymer of Polymerization 6 was processed into fibers and a non-woven fabric, and then

physical properties were determined and evaluated by a similar method to Example 1.

As the result, fibers having a single fiber fineness of 2.2D were obtained. The fibers had a single fiber strength of 1.0gf/D, a stretching rate of 351% and an initial tensile resistance of 8gf/D. The fibers were subject to carding and thermal adhesive treatments, to obtain a non-woven fabric having a basis weight of 20g/m². The non-woven fabric obtained at a thermal adhesion temperature of 126°C had a longitudinal strength of 4.10kgf/5cm width and one obtained at a thermal adhesion temperature of 134 °C had a longitudinal strength of 3.63kgf/5cm width. Softness of the non-woven fabric was normal at a thermal adhesion temperature of 126°C, but became hard at 134°C. Furthermore, fuming could be confirmed.

Therefore, it was seen that the fibers had a relatively low initial tensile resistance and that the non-woven fabric with use of the fibers had a decreased strength in the case of a high temperature treatment being carried out. Evaluated results are shown in Table 1.

Comparative Example 3

A fine fibrous non-woven fabric was prepared by a similar method to Example 3.

Propylene-ethylene copolymer of Polymerization 5 was extruded at a spinning temperature in an extruder of 310°C, and the extruded resin from spinning holes were blown on a web collecting device of a net conveyor by introducing heating air having a temperature of 400°C (pressure: 1.9kgf/cm²), to make a fine fibrous web by a melt-blowing method having a basis weight of about 25g/m². The heating air which was blown with the web was suction removed by a high-speed air stream suction removing device equipped on a lower part of a net conveyor. The said web became a non-woven fabric by inherent heat during spinning. Physical properties of the said non-woven fabric are shown in Table 2.

Comparative Example 4

Spinning and molding into a cylindrical filter were carried out by using propylene-ethylene copolymer by the similar method to Example 4. The tested results such as an accuracy of the obtained cylindrical filter are shown in Table 2.

Comparative Example 5

A spun-bonded continuous fibrous non-woven fabric was prepared by a similar preparation method to Example 2 by using propylene-ethylene copolymer of Polymerization 5.

A spinning temperature was 230°C and a drawing speed by an air sucker type drawer was 1607m/minute. The obtained continuous fibrous web had a single fiber fineness of 2.8D. Furthermore, a thermal adhering temperature of the said continuous fibrous web was 134°C.

The said non-woven fabric had a basis weight of 21g/m² and a longitudinal strength of 4.80kgf/5cm width. Furthermore, the said non-woven fabric had a longitudinal tensile strength at 5% stretched at 25°C of 1.49kgf/5cm width and a longitudinal tensile strength at 5% stretched at 80°C of 1.34kgf/5cm width. The said non-woven fabric had an inferior longitudinal tensile strength at 5% stretched at low and high temperatures compared to the above-mentioned Example 7. Particularly, decrease of the tensile strength at 5% stretched at a high temperature was much.

Comparative Example 6

On the other hand, a paper diaper was prepared by a similar method to Example 9, by using the non-woven fabric prepared in Comparative Example 5 as a surface material. However, its touch was stiff since the non-woven fabric became film-like partly.

Comparative Example 7

Sheath-core type composite monofilaments were prepared by a similar method to the above-mentioned Example 10 by using propylene-ethylene copolymer and polyethylene terephthalate used in Example 10. Also, a spinning temperature, a composite ratio and stretching conditions were same as Example 10.

The said composite monofilaments had a single fiber fineness of 252D, a single fiber strength of 4.0gf/D and a stretching rate of 52%. Furthermore, they had an initial tensile resistance of 29gf/D at 20°C and an initial tensile resistance of 20gf/D at 80°C.

The said composite monofilaments had a low strength and an initial tensile resistance both at the normal temperature and a high temperature.

Comparative Example 8

A net was prepared from the composite monofilaments of Comparative Example 7 by a similar method to Example 11.

5 A longitudinal strength of the obtained net was 5.05kgf/5cm width.

The net of this Comparative Example was judged to be unsuitable for use as a material of engineering work in which a high strength being required and an agricultural housing cover which being repeatedly used for applying and removing of net etc., since the net of this Comparative Example had a low strength.

10 As seen from Table 2, the cylindrical filter consisting of the melt-blown fine non-woven fabric had a finer fibrous diameter than that of the Comparative Example 4 spun under the same spinning conditions. Additionally, the cylindrical filter according to the invention was a filter having a good filtering accuracy and a superior heat resistance. The cylindrical filter according to the invention was judged to be useful as a filter not only for filtering use at the normal temperature but also at a high temperature as well as a filter for food and medical uses after thermal and sterilization treatments etc.

15 On the other hand, the cylindrical filter of the Comparative Example 4 had a high fibrous diameter as well as a poor filtering accuracy and a poor heat resistance. The said filter was judged to be unusable as a filter for food and medical uses after thermal and sterilization treatments etc., since the filter had a poor heat resistance.

Example 12

20 After an inside of a polymerization vessel having an inside volume of 100dm³ made of stainless steel equipped with a stirrer was substituted with nitrogen gas, a mixture of 50dm³ of n-hexane, a solution of 7.6mol (calculated as Al atom) of methyl aluminoxane in toluene (made by Toso-Akzo Co. Ltd., trade name: MMAO, concentration: 2mol/dm³), 1.48mmol of dimethyl silylene (2,3,5-trimethyl cyclopentadienyl)(2',4',5'-trimethyl cyclopentadienyl) hafnium dichloride which being chiral as metallocene and 0.05mmol of a *meso* compound, dimethyl silylene (2,3,5-trimethyl cyclopentadienyl)(2',3',5'-trimethyl cyclopentadienyl) hafnium dichloride was introduced with 1dm³ of toluene at 20°C. Then, a temperature within the polymerization vessel was raised to 27°C and hydrogen was supplied in order to make a hydrogen partial pressure within the polymerization vessel of 0.04MPa, thereafter propylene was supplied continuously for 4 hours in such an amount to keep the pressure within the polymerization vessel at 0.4MPa, to polymerize propylene. A temperature within the polymerization vessel was kept 27°C during polymerization. After polymerization was ended, non-reacted propylene was discharged from the inside of the polymerization vessel, thereafter 3dm³ of 2-propanol was introduced in the polymerization vessel and stirred at 30°C for 10 minutes, to deactivate the catalyst. Subsequently, 0.2dm³ of an aqueous hydrogen chloride solution (concentration: 12mol/dm³) and 8dm³ of methanol were added and heated at 60°C for 30 minutes. After the treatment, stirring was stopped and an aqueous phase part was removed from a lower part of the polymerization vessel, then similar operations were repeated by using the same amounts of an aqueous hydrogen chloride solution and methanol. Then, 0.02dm³ of an aqueous sodium hydride solution (concentration: 5mol/dm³), 3dm³ of water and 2dm³ of methanol were added, and stirred at 30°C for 10 minutes. After the treatment, stirring was stopped and an aqueous phase part was removed from a lower part of the polymerization vessel, then 8dm³ of water was added and stirred at 30°C for 10 minutes. After repeating the operation for removing an aqueous phase part twice, polymer slurry was took from the polymerization vessel, filtered and dried, to obtain polypropylene.

40 Short fibers having a single fiber fineness of 2.2D and a fibrous length of 51mm were produced by using polypropylene thus obtained as a core part and propylene-ethylene copolymer of Polymerization 1 as a sheath component of composite fibers by a similar method to Example 8 except for a spinning temperature of 280°C and a stretching roll temperature of 80°C. The said fibers had a single fiber strength of 3.5gt/D, a stretching rate of 252% and an initial tensile resistance of 30gt/D.

The short fibers were subject to thermal adhering treatment etc. by means of a carding and emboss roll type thermal adhering device similar to the above-mentioned Example 1, to obtain two thermally adhered non-woven fabrics at different thermal adhering temperatures.

50 The non-woven fabric made at a thermal adhering temperature of 126°C had a basis weight of 20g/m² and a longitudinal strength of 5.62kgf/5cm width. The non-woven fabric made at a thermal adhering temperature of 134°C had a basis weight of 20g/m² and a longitudinal strength of 7.12kgf/5cm width.

The said composite fibers had a thermal adhering property by thermal treatment at a temperature between above a softening point of the sheath component and below a melting point of the core component, as well as had a high single fiber strength and a high initial tensile resistance. Furthermore, the thermally adhered non-woven fabric with use of the said composite fibers was a non-woven fabric having a high strength and an extremely good softness, in both cases of treated at a low temperature and a high temperature.

The evaluated results are shown in Table 1.

Table 1

Example and Comparative Example	Example1	Example8	Example10	Example12	Comparative Example1	Comparative Example2	Comparative Example7	evaluation results			
								Polymerization Number			
								physical properties of fibers			
physical properties of nonwoven fabric	fineness (D)	2.2	2.2	261	2.2	2.2	2.2	262			
	single filament strength (g/DT)	2.3	3.0	6.9	3.5	1.2	1.0	4.0			
	initial tensile strength (g/DT)	20	28	45	30	9	8	29			
	initial tensile strength (g/DT:80°C)			37				20			
	strength (kg/5cm width) (processing temperature :126°C)	5.10	5.55		5.62	4.00	4.10				
	strength (kg/5cm width) (processing temperature :134°C)	6.92	6.68		7.12	3.91	3.63				
softness (processing temperature :126°C)	o	o		o	Δ	Δ					
	softness (processing temperature :134°C)	o	o		o	x	x				
		finishing	No	slightly	slightly	No	Yes	Yes	Yes		

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Example and Comparative Example		Examples3	Example4	Examples5	Examples6	Comparative Examples3	Comparative Example4	
Polymerization Number		4	4	4	4	5	6	
evaluation results	physical properties of nowoven	fibrous diameter (μm)	1.5	/	0.4	0.6	1.48	/
		strength (kgf/cm width) (5% stretching; 25°C)	1.42	/	0.86	/	1.29	/
		strength (kgf/cm width) (5% stretching; 80°C)	1.48	/	0.76	/	0.90	/
		fibrous diameter of inner layer (μm)	/	7.6	/	0.4	/	15.8
		fibrous diameter of intermediate layer (μm)	/	0.8	/	0.4	/	5.0
	physical properties of nonwoven fabric	fibrous diameter of outer layer (μm)	/	8.6	/	0.4	/	15.9
		filtering accuracy	/	1	/	0.6	/	8
		pressure resistant strength (kgf/cm ²)	/	10 or more than 10	/	10 or more than 10	/	10 or more than 10
		heat resistance	○	○	○	○	×	×
			○	○	○	○	×	×

Table 3

Example and Comparative Example	Polymerization Number	evaluation results			
		physical properties of fibers	physical properties of nonwoven fabric		
			strength (kg/5cm width) (5% stretching: 25°C)	strength (kg/5cm width) (5% stretching: 80°C)	strength (kg/5cm width) (processing temperature: 134°C)
Example 2	2	1.1	2.07	1.86	6.55
Example 7	2	1.4	2.03	1.79	6.42
Comparative Example 6	4	2.8	1.49	1.34	4.8

Table 4

Polymerization example	unit	Polymerization 1	Polymerization 2	Polymerization 3	Polymerization 4	Polymerization 5	Polymerization 6
total ethylene content	mol%	3.32	2.05	7.14	14.3	6.60	4.88
triad fraction (PEP)	PEP $\times 10^2$	2.78	1.66	6.70	10.44	4.60	4.00
triad fraction (EEE)	EEE $\times 10^2$	0.00	0.00	0.12	0.34	0.40	0.06
α,β -methylene carbon atom ratio (Ncf)	mol%	0.07	0.07	0.08	0.20	0.01	1.41
weight average molecular weight (M_w)	$M_w \times 10^{-4}$	18.9	18.6	36.3	7.2	19.0	26.8
molecular weight distribution (M_w/M_n)	-	2.3	2.2	1.7	2.2	4.1	2.0
melting point(T_m)	$^{\circ}\text{C}$	139.7	160.0	116.1	116.3	139.6	109.6

Advantage of the Invention

Fibers according to the invention was superior in a heat resistance during an adhering process, particularly when

used as fibrous moldings. The fibers according to the invention can be improved in the heat resistance while maintaining other effects, by using a specified propylene-ethylene copolymer as a raw material, compared to the conventional fibers containing conventional propylene-ethylene copolymer in the same proportion. For example, applications may be developed as filters etc. for which the use of the conventional propylene-ethylene copolymer fibers are restricted because of the required heat resistance. Furthermore, since strength and softness of the non-woven fabrics are extremely good, they are suitable as surface materials of sanitary napkins and throwaway diapers and have possible wider applications than the conventional fabrics made of propylene-ethylene fibers.

Claims

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1. Fibers comprising propylene-ethylene copolymer consisting of 0.01 to 15 mol% of ethylene units and 99.99 to 85 mol% of propylene units as at least one component, wherein

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a) a chain constitution of the copolymer found by means of nuclear magnetic resonance spectrum has the following relationships:

a-1) in three monomers chain units (triad) in main chains of the copolymer, there is a relationship of formula (I):

$$0.0070 \times C2 - 0.0020 \leq PEP \leq 0.0070 \times C2 + 0.0130 \quad (I)$$

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between a fraction of propylene unit - ethylene unit - propylene unit chain (PEP) and a total content of ethylene unit (C2), when PEP being positive, and

a-2) in three monomer chain units (triad) in main chains of the copolymer, there is a relationship of formula (II):

$$0 \leq EEE \leq 0.00033 \times C2 + 0.0010 \quad (II)$$

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between a fraction of three continuous ethylene units chain (EEE) and a total content of ethylene unit (C2), as well as

a-3) a ratio of total α,β -methylene carbon atoms ($N_{\alpha\beta}$) to total propylene units is within a range of 0 to 1.2 mol%,

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b) a weight average molecular weight (M_w) is 50,000 to 1,500,000, as well as

c) a ratio (M_w/M_n) of a weight average molecular weight (M_w) to a number average molecular weight (M_n) is 1.2 to 3.8.

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2. Fibers according to Claim 1, wherein there is a relationship of formula (III)

$$-8.1 \times C2 + 156.0 \leq T_m \leq -4.4 \times C2 + 165.0 \quad (III)$$

between a melting point of the copolymer (T_m) and a total content of ethylene units (C2).

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3. Fibers according to any of Claim 1 or 2, wherein fibers are composite fibers in which propylene-ethylene copolymer constitutes at least one component.

4. A non-woven fabric, wherein fibers according to any of Claims 1 to 3 being used.

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5. A non-woven fabric according to Claim 4, wherein the non-woven fabric being a continuous fibrous non-woven fabric obtained by a spun-bonding method.

6. A non-woven fabric according to Claim 4, wherein the non-woven fabric being a continuous fibrous non-woven fabric obtained by a melt-blowing method.

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7. A knitted textile, wherein fibers according to any of Claims 1 to 3 being used.

8. A filter, wherein fibers according to any of Claims 1 to 3 being used.

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9. A filter, wherein a non-woven fabric according to any of Claims 4 to 6 being used.

10. An absorbent article, wherein a non-woven fabric according to any of Claims 4 to 8 being used partly.